

Cell Culture Scale-Up in BioBLU[®] c Rigid-Wall, Single-Use Bioreactors

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Abstract

For cultivation of mammalian cells in biopharmaceutical research and manufacturing, single-use technology possesses several advantages to autoclavable material. Bioreactor scalability is critical to streamlining the adaptation of culture volumes during process development and manufacturing. We analyzed BioBLU Single-Use Vessels of different sizes (maximum working volumes of 0.25 L, 3.75 L, and 40 L) that are of geometrically similar stirred-tank design. We identified a scalable tip speed zone and an overlapping range of k₁ a values, which cover most mammalian cell culture needs. Using computational fluid dynamics simulations we determined the power numbers of the BioBLU bioreactors. Based on these data we scaled up a process for production of monoclonal antibodies (mAb) in CHO cells from 0.25 L to 3.75 L to 40 L by keeping constant P/V values (impeller power consumption per liquid volume) among the differently sized vessels. Similar cell growth curves and mAb production profiles were achieved at all three scales. In summary, this study demonstrates the excellent scalability

of the single-use bioreactors tested.

Vessel specifications

Table 1. BioBLU c Single-Use V	Vessel specifications
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	BioBLU 0.3c	BioBLU 3c	BioBLU 50c
Gas flow range SLPM	0.0007 - 0.08	0.002 – 1	0.04 - 7.5
(SLPH)	(0.04 - 5)	(0.12 - 60)	(2.4 – 450)
Maximum gas flow (VVM)	0.33	0.27	0.19
Total volume (L)	0.38	5	50
Working volume (L)	0.1 - 0.25	1.25 – 3.75	18 - 40
Working volume : total volume	0.66	0.75	0.80
V _{max} height* (mm)	82.0	220.7	428.0
Vessel inner diameter (ID) (mm)	67.0	147.1	337.0
Vmax height : vessel ID	1.2	1.5	1.3
Vessel height : vessel ID	1.8	2.0	2.0

Table 3. Tip speed vs. agitation.

Tip speed (m/s)	А	gitation (rpm)		
	BioBLU 0.3c	BioBLU 3c	BioBLU 50c	
0.1	58	29	12*	
0.2	116	58	24*	
0.3	174	87	36	Scalable
0.4	231	115	48	tip speed
0.5	290	145	60	zone:
0.6	347	174	72	0.3 – 0.7 m
0.7	405	200	84	
0.8	465	231*	96	•
0.9	520	260*	108	

Scope

The primary scope of this project was to investigate the scale-up capabilities of Eppendorf BioBLU Single-Use Vessels for cell culture applications from small to pilot scale.

Three bioreactor sizes were selected to represent approximately 10-fold scale-up between steps:

- > Small scale (max. 0.25 L): 4-fold DASbox[®] Mini Bioreactor System with BioBLU 0.3c Single-Use Vessels.
- Bench scale (max. 3.75 L): BioFlo[®] 320 bioprocess > control station with BioBLU 3c Single-Use Vessels.
- > **Pilot scale (max. 40 L):** BioFlo 320 bioprocess control station with BioBLU 50c Single-Use Vessels.

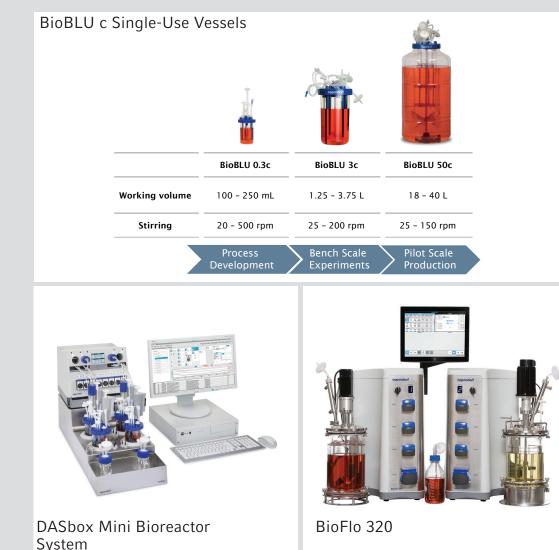


Figure 1. The equipment used in this study.

Oxygen transfer

Table 4. Measurement conditions for the determination of k, a values.

	BioBLU 0.3c					BioB	LU 3c		E	BioB	LU	50c			
	(Open pipe sparger)			(Macrosparger)			parger)	(Macrosparger)							
		Wo	orking	volume	e 0.25 L	V	Working volume 3.75 L			Working volume 40 L					
Tip speed (m/s)	0.3	0.4	0.5	0.6	0.7	0.3 0.4	0.5	0.6	0.7	0.3	0.4	0.5	0.6	0.7	
Agitation (rpm)	174	231	290	347	405	87 115	145	174	203	36	48	60	72	80	
VVM			Air flo	ow (S	LPM)		Air fl	ow (S	LPM)	A	ir fl	ow ((SLF	M)	
0.01				0	.0025			С	.0375					0.4	
0.03	0.0075					С	.1125					1.2			
=						·									

BioBLU 50c

2.0

4.0

6.0

0,15

0,1

Air flow rate (VVM)

k, a-based scalable zone

Maintaining a constant k_ia between vessels of different sizes is one of the frequently used strategies for cell culture scale-up. It is important to select equipment with similar

$\frac{72}{0.3 - 0.7}$ m/s	0.05 0.0125	0.1875
84	0.10 0.0250	0.375
96	0.15 0.0375	0.5625
108		
d vessel spec.)		
aall aultura	BioBLU 0.3c BioBLU 3c	9 8 7 7
cell culture	kta (h ⁻¹) kta (h ⁻¹) kta (h ⁻¹)	- 6 - 5 - 5
ale are v similar	ei 4 3 2 1 1	^r 4 − 3 − 2 − 1
SIIIIIdi	0 0 0,05 0,1 0,15 0 0,05 0,	,1 0,15 0 0,05
	Air flow rate (VVM) Air flow rate (VVI	
s – 0.7 m/s)	 0.3 m/s Tip speed 0.4 m/s Tip speed 0.5 m/s Tip speed 0.7 m/s Tip speed 	k _L a-base
lost	Figure 2. BioBLU Single-Use Vessel k _L a values	•

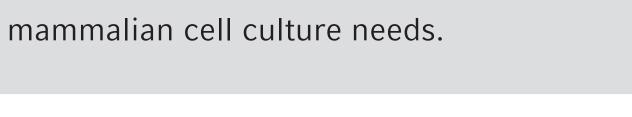
k_ia capabilities that offer sufficient overlapping so that the small scale success can be replicated in large scale. k_ia-based scale-up can be performed by maintaining constant k₁ a values among different vessels in the 0.8 – 6.0 h⁻¹ range, providing flexibility to accommodate different types of cell lines.

 V_{max} height = height from bottom of the vessel to liquid top surface at maximum vessel volume

 Table 2. BioBLU c Single-Use Vessels. Impeller specifications.

	BioBLU 0.3c	BioBLU 3c	BioBLU 50c
		BIUBLU SC	BIUBLU SUC
Impeller style	Pitched-blade	Pitched-blade	Pitched-blade
Impeller material	Polycarbonate	Polycarbonate	Polycarbonate
Impeller quantity	1	1	1
Impeller diameter (mm)	33	66	160
Impeller diameter : Vessel ID	0.5	0.5	0.5
Impeller height (mm)	25	50	120
Agitation (rpm)	20 - 500	25 – 200	25 – 150
Maximum tip speed (m/s)	0.9	0.7	1.3

The Eppendorf BioBLU single-use c vessels from small scale to pilot sca of geometrically and proportionally stirred-tank designs. A wide scalable tip speed zone (0.3 has been identified which covers most



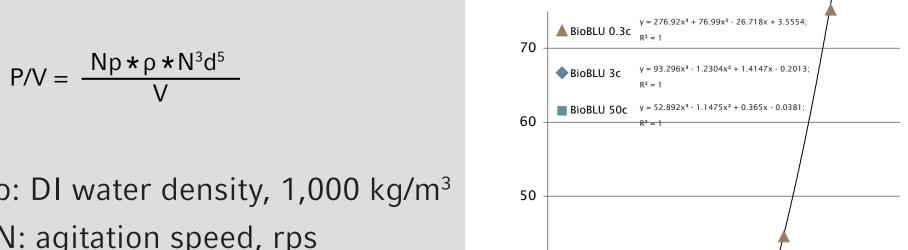


Using computational fluid dynamics (CFD) simulations the dimensionless power number Np was determined for different BioBLU vessels at different stirrer speeds.

Table 5. Power numbers obtained by CFD from
 0.3 – 0.7 tip speeds (one impeller, up flow, no gassing)

Bioreactor	Tip speed (m/s)	Np	Mean Np			different scales.	→ 0.3c (0.25 L) → 3c (3.75 L)
	0.3	2.64		ρ: DI water density, 1,000 kg/m ³	50	Bioreactor BioBLU 0.3c BioBLU 3c BioBLU 50c	250 <u></u>
	0.4	2.57		N: aditation should res		Tip speed (m/s) 0.30 0.47 0.58	~ ²⁰⁰
BioBLU 0.3	0.5	2.52	2.54	N: agitation speed, rps		Agitation (rpm) 174 137 69	
	0.6	2.49		d: impeller OD, m			
	0.7	2.46				Table 7. CHO cell culture. Experimental conditions for all	₹ ₁₀₀
	0.3	2.62		V: full working volume, m ³	à 30	scales.	
	0.4	2.58				CHO culture Conditions for all scales	50
BioBLU 3c	0.5	2.55	2.56			P/V 10.9 W/m ³	
	0.6	2.53				Air flow mode 3-Gas Auto	0 2 4 6
	0.7	2.52			Scale-up zone	Maximum gassing 0.19 VVM	Time (days)
	0.3	2.52			10	pH/deadband 7.0/0.1	
	0.4	2.52				DO 50 %	Figure 4. Scale-up of a mAb production
BioBLU 50c	0.5	2.52	2.52	Figure 3. Among the different vessels		Temperature 37°C	process with CHO cells. Viable cell density
	0.6	2.53		P/V can be kept constant in the range of	0 0.0 0.2 0.4 0.6	Working volume Maximum working volume	(top) and antibody concentration (bottom) we
	0.7	2.53		$10.0 - 18.2 \text{ W/m}^3$.	Tip speed (m/s)	(0.25 L I 3.75 L I 40 L)	analyzed at the different scales.

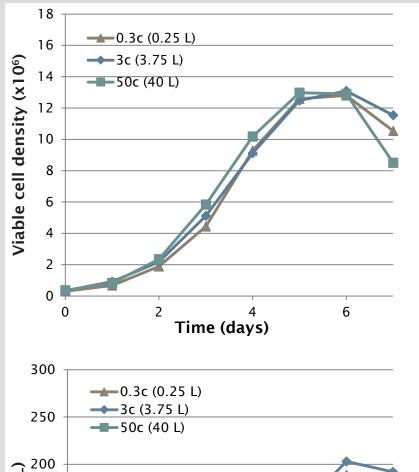
The purpose of determining Np is to calculate impeller power consumption per liquid volume (P/V, W/m³). Maintaining constant P/V between vessels is one of the most accepted strategies for scale-up. P/V can be converted from power number (Np) using the following equation:



CHO culture and mAb production was scaled up with a constant P/V of 10.9 W/m³. This lower P/V value within the scale-up zone was chosen to reduce tip speed/shearing. Scalable growth profiles and similar mAb production profiles were achieved from 0.25 L to 40 L.

Table 6. CHO cell culture. Tip speed and agitation at the

	0.3	2.64		ρ: DI water density, 1,000 kg/m ³	50	Bioreactor BioBLU 0.3c BioBLU 3c BioBLU 50c	
	0.4	2.57		N: agitation speed, rps		Tip speed (m/s) 0.30 0.47 0.58	
BioBLU 0.3	0.5	2.52	2.54	N. agriation speed, 1ps		Agitation (rpm) 174 137 69	/6u
	0.6	2.49		d: impeller OD, m			
	0.7	2.46				Table 7. CHO cell culture. Experimental conditions for all	۲ <u>۲</u> <u>۱</u> <u>۲</u>
	0.3	2.62		V: full working volume, m ³		scales.	
	0.4	2.58				CHO culture Conditions for all scales	50
BioBLU 3c	0.5	2.55	2.56			$\frac{10.9 \text{ W/m}^3}{10.9 \text{ W/m}^3}$	
	0.6	2.53			20	Air flow mode 3-Gas Auto	0 2 4 6
	0.7	2.52			Scale-up zone	Maximum gassing 0.19 VVM	Time (days)
	0.3	2.52			10	pH/deadband 7.0/0.1	
	0.4	2.52				DO 50 %	Figure 4. Scale-up of a mAb production
BioBLU 50c	0.5	2.52	2.52	Figure 3. Among the different vessels		Temperature 37°C	process with CHO cells. Viable cell density
	0.6	2.53			0 0.0 0.2 0.4 0.6	Working volume Maximum working volume	(top) and antibody concentration (bottom) were
	0.7	2.53		P/V can be kept constant in the range of	Tip speed (m/s)	(0.25 L I 3.75 L I 40 L)	analyzed at the different scales.
				10.0 – 18.2 W/m ³ .			



Conclusion

- > The Eppendorf BioBLU c Single-Use Vessels are of geometrically and proportionally similar stirred-tank designs.
- > A wide scalable tip speed zone has been identified which covers most mammalian cell culture needs.
- > All three vessel sizes offer a broad overlapping range of k_1 a values for excellent scalability.
- > P/V-based scale-up can be performed by maintaining constant P/V values among different vessels from 10.0 to 18.2 W/m³.
- > A CHO cell culture process was scaled-up from 0.25 L to 40 L using the constant P/V strategy. Similar cell growth curves and mAb production yield profiles were achieved at the different scales.

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